

1        **Microwave flow and conventional heating effects on the physicochemical**  
2        **properties, bioactive compounds and enzymatic activity of tomato puree**  
3        [Journal Science Food Agriculture. 97\(3\): 984-990. doi: 10.1002/jsfa.7824.](#)

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13  
14        **ABSTRACT**

15        **BACKGROUND:** Thermal processing causes a number of undesirable changes in  
16        physicochemical and bioactive properties of tomato products. Microwave (MW)  
17        technology is an emergent thermal industrial process that offers a rapid and  
18        uniform heating, high energy efficiency, and high overall quality of the final  
19        product. The main quality changes of tomato puree after a pasteurization at  $96 \pm 2$   
20        °C for 35 s, provided by a semi industrial continuous microwave oven (MWP)  
21        under different doses (low power/long time to high power/short time) or by  
22        conventional method (CP) were studied.

23        **RESULTS:** The results showed that all heat treatments reduced color quality, total  
24        antioxidant capacity and vitamin C, with a greater reduction in CP than in MWP.  
25        On the other hand, use of a MWP, in particular, high power/short time (1900

26 **W/180 s, 2700 W/160 s and 3150 W/150 s) enhanced the viscosity, lycopene**  
27 **extraction and decreased the enzyme residual activity better than with CP**  
28 **samples. For tomato puree, polygalacturonase was the more thermos resistant**  
29 **enzyme, and could be used as an indicator of pasteurization efficiency.**

30 **CONCLUSION: MWP was an excellent pasteurization technique that provided**  
31 **tomato puree with improved nutritional quality, reducing process times compared**  
32 **to the standard pasteurization process.**

33

34 **Keywords: Carotenoids; Viscosity; Vitamin C; Thermal treatment; Smoothie.**

35

## 36 1. INTRODUCTION

37 Tomato (*Lycopersicon esculentum* L.) is widely grown around the world and becoming  
38 increasingly popular, both fresh and processed. Tomato and tomato products have very  
39 high levels of bioactive compounds such as carotenoids, especially lycopene, followed  
40 by  $\beta$ -carotene<sup>1</sup>. Dietary intake of tomatoes and tomato products containing lycopene,  
41 has been shown to reduce the risk of prostate cancer.<sup>2</sup> Processed products contain more  
42 lycopene than fresh foods because thermal treatment causes transformation of the *trans*  
43 isomers in *cis* form.<sup>3</sup>

44 All tomato products are usually prepared by thermal processing for inactivating  
45 natural degrading enzymes and microorganisms that may cause unwanted modification  
46 during their storage.<sup>4</sup> But this processing causes a number of undesirable changes in  
47 physicochemical properties of products and must be applied without compromising  
48 food safety, nutritional quality and shelf life.<sup>5,6</sup> MW technology is an emergent thermal  
49 industrial process to achieve this purpose. It enhances microbial destruction and help to  
50 maintain the product quality.<sup>7</sup> In comparison with conventional heating methods, the  
51 industrial MW oven offers a rapid and relatively uniform heating, high energy  
52 efficiency, reduced space utilization, precise process control, fast start-up, shutdown  
53 conditions and high overall quality and safety of the final product.<sup>6,8</sup> Several studies  
54 have assessed the safety as well as nutrient loss associated with MW cooking, and  
55 antioxidant activity of strawberry and kiwifruit apuree.<sup>9,10</sup> Additionally, high-  
56 power/short-time MW processes reduced the adverse thermal degradation in food  
57 quality while ensuring food safety because of the nutrient characteristics of product  
58 being more sensitive to time than to temperature.<sup>11</sup> In this way, the aim of the present  
59 work was to investigate quality parameter changes such as vitamin C, lycopene,  $\beta$ -  
60 carotene, total phenolics content (TPC), and total antioxidant capacity (TAC), as well as

61 color parameters, viscosity and enzymatic activity of a tomato puree after CP and MWP  
62 using different doses (powers and times) of processing.

63

## 64 **2. MATERIALS AND METHODS**

65

### 66 **2.1. Plant materials**

67 Tomato (*Lycopersicon esculentum* Mill., Moneymaker cv.) were grown in greenhouse  
68 under Mediterranean climate (Mazarrón, Murcia, Spain). They were harvested  
69 according to commercial maturity stage, obtaining  $4.73 \pm 0.07$  °Brix and  $44.94 \pm 0.19$   
70 h°. Fruits free from defects and with a similar visual appearance were blended with a  
71 commercial thermomix (Vorwerk Elektrowerke, Model TM 31-1, France) in order to  
72 obtain a puree.

73

### 74 **2.2. Thermal treatment**

75 600 mL of puree samples were heated in the above cited thermomix (conventional  
76 pasteurization, (CP). Alternatively, samples for each MW pasteurization (MPW)  
77 treatment were placed in 3 tempered and extra resistant MW glasses were used  
78 (Hostelvia, Vicrila, Leioa, Spain). These glass beakers, containing each one 200 mL of  
79 tomato puree was treated in an innovative semi-industrial prototype of continuous MW  
80 oven (Sairem Ibérica S.L. SI-MAQ0101, Barcelona, Spain) with a power control from 0  
81 to 3,000 W (Fig. 1). Based on our preliminary studies several appropriate  
82 temperature/time combinations of MWP were selected with following conditions:

83         Low power/long time (390 W/848 s, 510 W/805 s, 770 W/460 s), medium  
84 power and time (980 W/848 s, 1,640 W/805 s, 1,700 W/230 s) and high power/short  
85 time (1,900 W/180 s, 2,700 W/160 s and 3,150 W/150 s). In both CP and MWP

86 processing the final temperature in all the treatments was  $96 \pm 2^\circ\text{C}$  and they remained at  
87 this temperature for 35 s.

88 After both kinds of pasteurization, the samples were packaged aseptically into  
89 plastic tubes and rapidly cooled ( $5^\circ\text{C}$ ) with an ice-water bath and then analyzed before  
90 (control) and after thermal treatments. For each heating method, the full experiment was  
91 conducted independently three times, each one constituting a repetition which was  
92 analysed.

93

### 94 **2.3. Analysis and quality determination**

#### 95 *Physical quality analysis*

96 Color: The color of the samples was monitored by photo-colorimeter (Minolta CR-300,  
97 Ramsey, NJ, USA). Color was expressed as Hunter L\*, a\*, b\* and hue angle ( $h^\circ = \tan^{-1}$   
98  $b^*/a^*$ ).

99 Viscosity: Viscous flow tests were determined in triplicate with a controlled shear  
100 rate/stress rheometer (AR G-2, TA Instruments, U.K) at  $20^\circ\text{C}$ . Viscous flow tests were  
101 performed by using a shear rate range between 1 and  $100\text{ s}^{-1}$ .

102

#### 103 *2.3.2 Chemical quality attributes*

104 Titratable acidity (TA), soluble solids content SSC and pH were analyzed as described  
105 by Aguayo et al.<sup>12</sup>

106

#### 107 *Total phenolic compounds (TPC) and total antioxidant activity (TAC)*

108 TPC was measured following by Swain and Hillis<sup>13</sup> method using a Multiscan plate  
109 reader (Tecan Infinite M200, Männedorf, Switzerland). TPC was expressed as mg  
110 chlorogenic acid equivalents (ChAE)  $\text{kg}^{-1}$  fresh weight (FW).

111 TAC was assessed using the Ferric Reducing Antioxidant Power (FRAP)  
112 technique<sup>14</sup> with the same device as for TPC. Results were expressed as mg ascorbic  
113 acid equivalent (AAE) kg<sup>-1</sup> (FW).

114

#### 115 *Total vitamin C*

116 The ascorbic acid (AA) determination was performed as described by Falagán et al.<sup>15</sup> 10  
117 mL of puree were mixed with 10 mL of a solution containing 45 g L<sup>-1</sup> of  
118 metaphosphoric acid and 7.2 g L<sup>-1</sup> of DTT (DL-1, 4-dithiotreitol). The mixture was  
119 centrifuged at 22,100 × g for 15 min at 4 °C (Eppendorf, AG 22331, Germany). The  
120 analysis of vitamin C was carried out by HPLC (Waters 2695, Detector UV-V 2687,  
121 Milford, USA). Detection was performed with an UV-visible spectrophotometer  
122 (Hewlet Packard, Model 8453, Columbia, USA) at 260 nm. Vitamin C was quantified  
123 through a calibration curve made with AA standards and results were expressed as mg  
124 (AA) kg<sup>-1</sup> FW.

125

#### 126 *Carotenoids*

127 Carotenoids were measured according to the method of Nagata and Yamashita<sup>16</sup> with  
128 the slight modifications. 5 mL of smoothie were mixed with 20 mL acetone-hexane  
129 (4:6). Two phases separated and the upper phase was taken for lycopene and β-carotene  
130 measurements at 663, 645, 505 and 453 nm in a UV-visible spectrophotometer (Hewlet  
131 Packard, Model: 8453, Columbia, EEUU). Lycopene and β-carotene were calculated  
132 according to the following equations:

$$133 \quad \text{Lycopene} = -0.0458 A_{663} + 0.204 A_{645} + 0.372 A_{505} - 0.0806 A_{453}$$

$$134 \quad \beta\text{-carotene} = 0.216 A_{663} - 1.22 A_{654} - 0.304 A_{505} + 0.452 A_{453}$$

135 Results were expressed as mg lycopene or β-carotene kg<sup>-1</sup> FW.

136

137 *Peroxidase (POD)*

138 POD activity was measured using the method described by Elez-Martínez et al.<sup>17</sup> 0.009  
139 mL enzyme extract, 0.243 mL of phosphate buffer 0.05 M, 0.018 mL of phenildiamina  
140 (10 g kg<sup>-1</sup>), and 0.009 mL of H<sub>2</sub>O<sub>2</sub> (15 g kg<sup>-1</sup>) in a 96-well polystyrene flat-bottom plate.  
141 The absorbance was measured at 509 nm for 10 min at 25 °C by using the multiscan  
142 plate reader cited above.

143

144 *Pectin methylesterase (PME)*

145 PME activity was determined according to Ratneret et al.<sup>18</sup> with slight modifications. A  
146 2.5 mL sample of puree was homogenized with 10 mL of sodium chloride 0.2 M. After  
147 filtering the homogenate by cheesecloth, 2.5 mL of it was mixed with 15 mL pectin (10  
148 g L<sup>-1</sup>). This solution was adjusted to pH 7.0 with 1N NaOH and the pH was kept at 7.0  
149 during 10 min using 0.01 N NaOH. One PME U can be expressed as the amount of  
150 enzyme that produces 1 nmol of acid per minute at pH 7.0 and 22 °C.

151

152 *Polygalacturonase (PG)*

153 PG activity was measured according to Aguiló-Aguayo et al.<sup>4</sup> with slight modifications.  
154 2 mL of sample was homogenized two times in 15 and 10 mL of cold acetone for 30  
155 and 15 min, respectively. The supernatant was again decanted and replaced with 5 ml of  
156 tris hydroxymethyl aminomethane buffer (0.2 M), pH 7.0, including 0.5 g L<sup>-1</sup> of  
157 sodium metabisulfite, 10 g L<sup>-1</sup> PVPP and 1M NaCl. The extraction was carried out  
158 during 2 h in an orbital shaker (Stuart, Staffordshire, UK) at 200 × g in darkness inside a  
159 polystyrene box with ice at 4 °C. The homogenate was centrifuged at 20,000 × g for 15  
160 min at 4 °C. The supernatant was used as enzyme extract. The PG activity was

161 quantified according to Gross.<sup>19</sup> The substrate was constituted of 0.6 mL of a solution  
162 containing 4 g L<sup>-1</sup> (w/v) polygalacturonic acid in 0.05 M sodium acetate buffer (pH 4.5)  
163 and the reaction was carried out by adding 0.15 mL of enzyme extract, followed by  
164 incubation at 37 °C for 10 min with shaker of 30 rpm. The reaction was stopped with 2  
165 mL of 10 mM borate buffer at pH 9 and 0.4 mL of 10 g L<sup>-1</sup> (w/v) cyanoacetamide. The  
166 mixture was put in a boiling water bath (100 °C) for 10 min and then chilled by ice. 200  
167 µL of extraction was put in a 96-well polystyrene flat-bottom plate the well. The  
168 absorbance of samples was measured. The absorbance was read at 276 nm using the  
169 same device as for POD at 22 °C. The quantity of reducing groups formed was  
170 determined using a calibration curve made with D-galacturonic acid and the enzyme  
171 activity was expressed as mM of galacturonic acid released per min. One unit (U) of PG  
172 activity was defined as the amount of enzyme that yielded 1 mM of reducing groups per  
173 min.

174 For all analysis, each of the three replicates was analyzed by triplicate.

175

#### 176 *2.4. Statistical analysis*

177 Data were analyzed in a randomized design with three replicates per treatment. Data  
178 were subjected to one-way analysis of variance ( $p \leq 0.05$ ) using Statgraphic Plus 5.1,  
179 Manugistic Inc, Rockville, MD, USA). Mean values were compared by multiple range  
180 least significant difference test to identify significant differences among treatments. A  
181 Pearson's correlation analysis was performed to corroborate relationships between  
182 specific parameters.

183

### 184 **3. RESULTS AND DISCUSSION**

185 *Color*

186 The effects of thermal treatment on tomato puree color are shown in Table 1. L\* values  
187 decreased after any thermal treatment. The lowest L\* reduction was obtained using high  
188 MW power/short time dose of processing. This reduction was only of 5.6% using 3,150  
189 W/150 s compared to unheated samples. In this same trend, h° increased in samples  
190 thermally treated being higher in CP than in MWP treated under high power/short time,  
191 indicating a changing of color from red to orange. Lower h° is preferred as the best  
192 color properties in tomato.<sup>20</sup> Results in this experiment showed that the use of MWP  
193 was able to keep the tomato puree color better than CP. The results agree with results  
194 obtained in orange juice<sup>21</sup> and kiwi fruit puree<sup>10</sup> treated by MW. The main red colored  
195 tomato pigment is *trans* lycopene and smaller amounts of *cis*-isomers (yellow colored  
196 pigment in tomato) and other carotenoids. In this case, Pearson correlation coefficient  
197 showed a positive correlation between the amount of lycopene and redness (a\*) of  
198 treated samples (0.758). Thermal processing leads to isomerization of lycopene from  
199 *trans* to *cis*-form<sup>3</sup> and since the redness of tomato depends on the level of *trans*-  
200 lycopene<sup>22</sup> therefore, severe thermal treatment leads to decreasing of the redness.

201

202

203 *Viscosity*

204 This is an important quality attribute to determine the overall quality of processed  
205 tomato products which is influenced by the presence of pectin and inactivation of PME  
206 and PG after thermal treatment.<sup>23,24</sup> From a rheological point of view, tomato puree can  
207 be considered as a weak gel<sup>23</sup> and its viscosity is not stable and influenced by changing  
208 the degree of shear rate. The effect of MWP and CP on tomato puree viscosity (shown  
209 in low shear rate) is presented in Fig. 2. There was an increase ( $p < 0.05$ ) in the viscosity  
210 of the samples when pasteurized by both methods compared to unheated puree. The

211 MWP, in particular, high power combined with low time, provided the higher viscosity  
212 compared to CP and unheated samples. For low shear rates, the viscosity value ranged  
213 from 81.73 to 53.54 Pa.s for MWP puree compared to 43.85 Pa.s CP and 21.33 Pa.s for  
214 CP and unheated samples, respectively. This viscosity decreased for higher shear rates  
215 and reached 4 and 2.5 Pa.s in all treatments, at a shear rate of  $100\text{ s}^{-1}$ . Due to disruption  
216 of the samples treated cell wall during thermal treatment, the soluble pectin could be  
217 increased. In the current research and several other studies, an increase in viscosity of  
218 tomato products was found with increasing pectin content.<sup>25,26</sup> On the other hand,  
219 different inactivation levels of PME and PG during pasteurization of puree as well as  
220 varietal characteristics and the maturity stage of fruits at processing have an influence  
221 on the viscosity.<sup>27</sup> According to our results, the reduction of PME and PG activity by  
222 both thermal treatment methods lead to increased viscosity.

223

#### 224 *SSC, pH and TA*

225 The SSC range between 4.73 and 5.27 °Brix, pH values 4.11 to 4.26 and TA had a mean  
226 of 0.37% in unheated and heated samples without significant differences (data not  
227 shown). The literature reported that temperature and treatment time had no effect on pH  
228 and °Brix of CP orange juice.<sup>28</sup>

229

#### 230 *TPC*

231 The initial TPC in fresh tomato puree was 424 ChAE  $\text{mg kg}^{-1}$  (Table 2). The range from  
232 268 to 523  $\text{mg kg}^{-1}$  reported for different tomato juices.<sup>29</sup> In this work, after any heat  
233 treatment the TPC was in the range between 430.6 and 441.2 ChAE  $\text{mg kg}^{-1}$  without  
234 significant difference between unheated or heated treatments. Similarly to our results it  
235 was reported a non-significant enhancement of TPC after CP at 90 °C for 30 or 60 s in

236 tomato juice<sup>30</sup>. Since POD is involved in the oxidative degradation of phenolic TPC<sup>31</sup>,  
237 inactivation of POD avoids degradation of TPC during thermal processing. Also the  
238 slight TPC enhancement could be attributed to the disruption of cell wall during  
239 heating, therefore making phenolics more accessible for extraction.<sup>5</sup>

240

#### 241 *TAC*

242 The TAC was influenced by type of heating and decreased significantly ( $p<0.05$ )  
243 compared to unheated samples Table 2. As previously reported, TAC in MW treated  
244 tomatoes or tomato paste<sup>32</sup> or watermelon juice<sup>33</sup> is strongly decreased by heating. In the  
245 current work initial TAC in unheated samples was 725.2 mg AAE kg<sup>-1</sup>. The highest  
246 TAC degradation (around 28%) was found in the CP treated puree, whereas this level  
247 was only 6% in MWP samples treated by highest power/short time of processing. These  
248 results showed that at similar temperature ( $96 \pm 2$  °C) MWP maintained a better TAC  
249 than CP. In the same way, Stratakos et al.<sup>34</sup> reported the TAC, in heated tomato juice  
250 was higher for MWP compared to the CP at 85 °C. TAC depends on the extract and the  
251 intensity of the heating applied to tomato samples.<sup>35</sup> In our results, the highest power  
252 (1,900 to 3,150 W) combined with shorter duration (180 to 150 s) maintained the TAC  
253 better than low power (390 to 770 W) combined with higher duration (848 to 460 s).  
254 Arslan et al.<sup>36</sup> found that MW drying at 700 W offered a lower TAC destruction than  
255 MW at 200 W. In summary, when comparing the efficacy of the MWP versus CP,  
256 advantage for keeping the TAC of tomato puree was found, in particular, using highest  
257 power and lowest time.

258

#### 259 *Vitamin C*

260 The vitamin C amount in MWP and CP purees is presented in Table 2. Vitamin C  
261 content in fresh tomato is between 80 and 163 mg kg<sup>-1</sup> FW<sup>37</sup>, depending on the cultivar,  
262 the cultivation conditions and ripening stage.<sup>38</sup> The vitamin C was degraded by 40% in  
263 CP, whilst in MWP puree was only 10% (highest power/short time) to 28% (low  
264 power/long time) showing that vitamin C of puree was maintained better by MWP than  
265 by CP. Similar results were obtained for strawberry puree showing that degradation of  
266 vitamin C in MWP (90 °C for 7 or 10 s) samples was from 4 to 22%, while achieving  
267 62% by CP.<sup>9</sup> After MW treatment of potato<sup>39</sup>, spinach<sup>40</sup> and apricot<sup>41</sup> the total AA  
268 content decreased with increasing processing time at a constant temperature. Decreasing  
269 of vitamin C occurs just after heating because this vitamin is very sensitive to heat.<sup>42</sup>

270

#### 271 *Carotenoids*

272 The lycopene levels ranged from 15.94 in unheated to 20.07 mg kg<sup>-1</sup> in MWP puree  
273 (Table 2), being slightly but significantly enhanced by both heating methods in  
274 particular samples treated under high power MWP doses compared to CP samples.  
275 Since it is the main carotenoid responsible for the intense redness of the tomato, its level  
276 is considered as a quality index.<sup>44</sup> Heating leads to isomerization of lycopene from  
277 trans-form to cis-form and a more efficient extraction from the matrix by breaking down  
278 cell walls, therefore making lycopene more accessible.<sup>45</sup> Temperature kinetics play an  
279 important role in lycopene bio-accessibility as rapid heating of tomato puree can lead to  
280 higher accessibility compared to a slow temperature increase.<sup>46</sup> In this experiment, we  
281 can add that even if obtaining the same final temperature of pasteurization, the kinetic  
282 of MWP power doses is also very important and the combination of highest power/short  
283 time of processing improved the lycopene content. On the contrary, other authors found  
284 that the lycopene content was stable in tomatoes under different thermal treatments.<sup>47,23</sup>

285 For the cells that were not disrupted during the puree preparation, such as tomato skin  
286 cells, a longer heating time or higher temperature may be needed to disrupt the cell  
287 walls sufficiently to release all the lycopene from cells.<sup>48</sup> These authors showed that  
288 long-time/low temperature and short-time/high temperature can have the same effects  
289 on the tomato matrix. Also, the lycopene remains relatively stable during food  
290 processing, except at high temperature or long heating time.<sup>43</sup>

291 The  $\beta$ -carotene content was also affected by heating method, and increased after  
292 pasteurization compared to unheated samples (Table 2). The raw tomato had the lowest  
293  $\beta$ -carotene content (6.76 mg kg<sup>-1</sup>). This value increased to reach 7.37 and 9.60 mg kg<sup>-1</sup> in  
294 CP and MWP, respectively. It has been reported that there is an enhanced  
295 bioavailability of carotenoids after heat treatment in tomato<sup>49</sup> and pumpkin<sup>50</sup> when  
296 compared to fresh sample. As explained with lycopene content, heat treatment might  
297 improve  $\beta$ -carotene bioavailability by breaking down of the cellulose structure of the  
298 plant cell walls.<sup>51</sup>

299

### 300 *Enzyme activity*

301 POD is responsible for enzymatic browning and can lead to reduction in nutritive  
302 quality, color, and flavor in many plant foods, being a common indicator of enzyme  
303 inactivation because of its high thermal stability.<sup>4</sup> Both thermal treatments reduced the  
304 POD activity in tomato puree (Table 3). In comparison to CP, highest MWP power  
305 combined with short time of processing induced a higher decrease of POD activity. A  
306 similar POD inactivation has been reported at 90 °C for 30 or 60 s in apple juice.<sup>52</sup>

307 PME and PG are the most important enzymes affecting the processed tomato  
308 quality playing an important role in the pectin degradation in the primary cell wall and  
309 middle lamella.<sup>53</sup> PME also leads the pectin chain to be susceptible to more pectin

310 degradation by PG reducing the tomato viscosity.<sup>54</sup> Consequently PME and PG  
311 inactivation is needed to avoid quality losses.

312 In this experiment, MWP decreased the PME residual activity better than CP  
313 (Table 3). PME activity was significantly affected by the highest power/short time  
314 MWP treatment (12%). Similarly, in the current work, PME inactivation in orange juice  
315 was faster by MW heating than by CP.<sup>21,55</sup> In most industrial uses the PME residual  
316 activity remaining below 10% guarantees the tomato quality and shelf-life.<sup>4</sup>

317 The PG is present in tomato as PG<sub>1</sub> (thermo-stable form), inactivated at 90 °C, 5  
318 min and PG<sub>2</sub> (thermo-labile form), inactivated at 65 °C, 5 min.<sup>54,56</sup> The PG activity  
319 decreased as a function of thermal treatment (Table 3). The major reduction (71%) was  
320 found in MWP at 3,150 W/150 s, whereas only 52 and 55% inactivation was reached at  
321 390 W/848 s and CP, respectively. The high PG activity after all treatments could be  
322 attributed to the presence of PG<sub>1</sub> and prolonged heating leads to complete inactivation  
323 of PG.<sup>57</sup> Results in the present study indicated that MWP might improve PME and PG  
324 inactivation through high power and reduced processing time more than with CP.  
325 According to Pearson coefficient, there was a negative correlation between residual PG  
326 and PME enzyme activity and viscosity of treated smoothies (-0.895 and -0.876,  
327 respectively). This correlation showed that the viscosity strongly was influenced by the  
328 reduction in PG and PME enzyme activity<sup>4</sup>.

329 As reported in fruit purees and strawberry puree, the POD activity in tomato  
330 puree was better inactivated than PG and PME in a microwaved product.<sup>57</sup> For this  
331 tomato puree, PG was the more thermo-resistant enzyme, and could be used as an  
332 indicator of pasteurization efficiency.

333

334 **CONCLUSION**

335 Physicochemical properties of tomato puree, especially color, were greatly influenced  
336 by heat treatments. MWP was able to preserve tomato puree redness, one of the major  
337 quality indicators, better than CP. Generally, MWP induced an enrichment of health-  
338 promoting compounds, leading to more retention of antioxidant capacity and vitamin C  
339 and enhancing lycopene content. PME and PG enzyme activities were highly decreased  
340 by MWP, in particular when high power/short time doses were used, resulting in a  
341 better viscosity. For all these reasons the semi-industrial continuous MW heating  
342 method studied, using high power combined with short processing time, could be  
343 recommended as an emergent pasteurization technique for maintaining quality of  
344 tomato puree.

345

#### 346 **ACKNOWLEDGEMENTS**

347 This work was financially supported by MINECO-FEDER (AGL2013-48830-C2-1-R).

348

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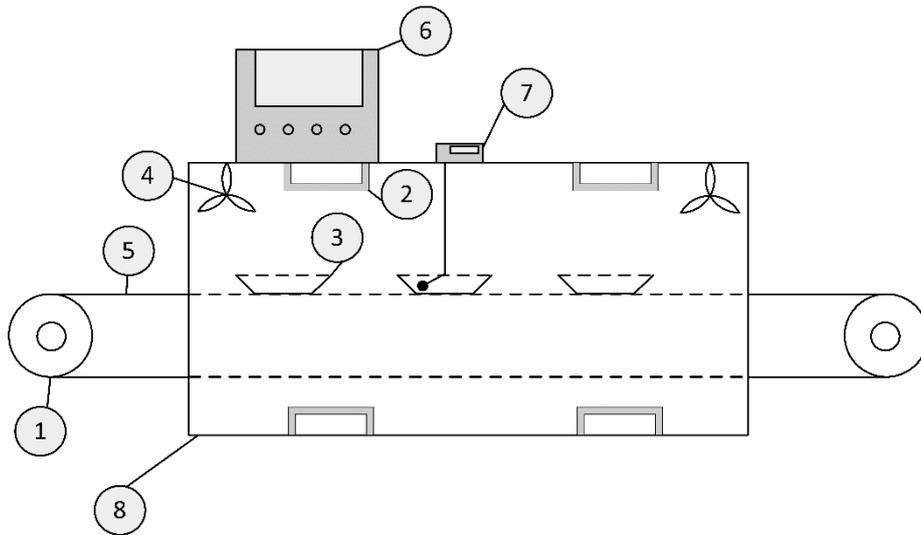
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523 **Figure 1.** Semi-industrial microwave oven, process diagram.

524 1.- Motor

525 2.- Magnetron

526 3.- Sample

527 4.- Fan

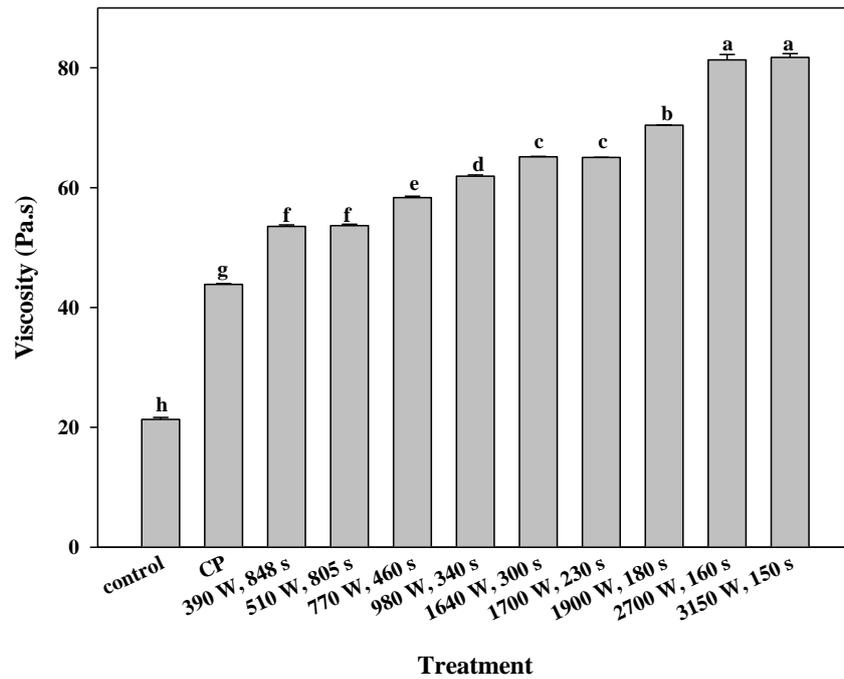
528 5.- Conveyor belt

529 6.- Control process

530 7.- Fiber optical temperature sensor

531 8.- Microwave chamber

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534 **Figure 2.** Viscosity in unheated (control), conventional (CP) and microwave (MWP)

535 pasteurized tomato puree. Different letters indicate significant differences among mean

536 values ( $p < 0.05$ ).

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538

**Table 1.** Color changes in unheated (control), conventional (CP) and microwave (MWP)

539

pasteurized tomato puree

	<b>Treatments</b>	<b>L*</b>	<b>Hue angle</b>
<b>MWP</b>	Untreated	39.60 ± 0.17 <sup>a</sup>	44.94 ± 0.19 <sup>d</sup>
<b>Doses</b>	CP	33.00 ± 0.38 <sup>f</sup>	48.44 ± 0.10 <sup>a</sup>
<b>Low</b>	390 W-848 s	35.36 ± 0.12 <sup>e</sup>	48.70 ± 0.80 <sup>a</sup>
	510 W-805 s	35.80 ± 0.12 <sup>de</sup>	47.45 ± 0.19 <sup>ab</sup>
	770 W-460 s	35.84 ± 0.22 <sup>de</sup>	47.03 ± 0.23 <sup>abc</sup>
<b>Medium</b>	980W-340 s	36.38 ± 0.41 <sup>cd</sup>	46.61 ± 0.50 <sup>abc</sup>
	1640 W-300 s	36.39 ± 0.37 <sup>cd</sup>	46.18 ± 0.64 <sup>abc</sup>
	1700 W-230 s	36.82 ± 0.40 <sup>bc</sup>	45.67 ± 0.86 <sup>bc</sup>
<b>High</b>	1900 W-180 s	36.93 ± 0.14 <sup>bc</sup>	45.45 ± 0.27 <sup>bc</sup>
	2700 W-160 s	37.08 ± 0.09 <sup>bc</sup>	45.12 ± 0.60 <sup>bc</sup>
	3150 W-150 s	37.36 ± 0.25 <sup>b</sup>	45.06 ± 0.19 <sup>c</sup>

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Values are mean ± standard error (n=3). Different letters in the same column indicate significant differences among mean values of different treatments ( $p < 0.05$ ). "ns" means there are no significant differences. Low MWP: Microwave pasteurization at low power and long time. Medium MWP: Microwave pasteurization at medium power and medium time. High MWP: Microwave pasteurization at high power and short time.

544 **Table 2.** Total antioxidant capacity (TAC, mg AAE kg<sup>-1</sup>), total phenolic compound (TPC, ChAE mg kg<sup>-1</sup>),  
 545 Vitamin C (mg kg<sup>-1</sup>), lycopene and β carotene (mg kg<sup>-1</sup>) in unheated (control), conventional (CP) and  
 546 microwave pasteurized (MWP) tomato puree.

	Treatment	TAC	TPC	Vitamin C	Lycopene	β-carotene
<b>MWP</b>	Untreated	725.2 ± 0.17 <sup>a</sup>	424.0 ± 0.47 <sup>ns</sup>	100.0 ± 0.02 <sup>a</sup>	15.94 ± 0.86 <sup>e</sup>	6.76 ± 0.90 <sup>ns</sup>
<b>Doses</b>	CP	519.4 ± 0.25 <sup>g</sup>	430.6 ± 0.02 <sup>ns</sup>	59.8 ± 0.02 <sup>g</sup>	17.19 ± 0.88 <sup>de</sup>	7.37 ± 0.06 <sup>ns</sup>
<b>Low</b>	390 W-848 s	559.1 ± 0.40 <sup>f</sup>	430.0 ± 0.36 <sup>ns</sup>	72.4 ± 0.06 <sup>f</sup>	17.66 ± 0.07 <sup>cd</sup>	9.08 ± 0.04 <sup>ns</sup>
	510 W-805 s	559.5 ± 0.25 <sup>f</sup>	430.7 ± 0.35 <sup>ns</sup>	72.4 ± 0.02 <sup>f</sup>	17.98 ± 0.22 <sup>cd</sup>	9.11 ± 0.63 <sup>ns</sup>
	770 W-460 s	560.8 ± 0.43 <sup>f</sup>	430.7 ± 0.37 <sup>ns</sup>	73.5 ± 0.06 <sup>f</sup>	17.99 ± 0.15 <sup>cd</sup>	9.08 ± 0.53 <sup>ns</sup>
<b>Medium</b>	980W-340 s	578.8 ± 0.44 <sup>e</sup>	431.7 ± 0.37 <sup>ns</sup>	77.4 ± 0.01 <sup>e</sup>	18.05 ± 0.12 <sup>cd</sup>	9.49 ± 0.50 <sup>ns</sup>
	1640 W-300 s	615.9 ± 0.23 <sup>d</sup>	432.6 ± 0.40 <sup>ns</sup>	87.0 ± 0.08 <sup>d</sup>	18.15 ± 0.21 <sup>bcd</sup>	9.54 ± 0.21 <sup>ns</sup>
	1700 W-230 s	619.6 ± 0.37 <sup>d</sup>	433.1 ± 0.63 <sup>ns</sup>	88.1 ± 0.03 <sup>cd</sup>	18.47 ± 0.07 <sup>bcd</sup>	9.56 ± 0.10 <sup>ns</sup>
<b>High</b>	1900 W-180 s	663.1 ± 0.20 <sup>c</sup>	440.3 ± 0.33 <sup>ns</sup>	89.0 ± 0.05 <sup>bc</sup>	19.17 ± 0.36 <sup>abc</sup>	9.57 ± 0.34 <sup>ns</sup>
	2700 W-160 s	682.6 ± 0.38 <sup>b</sup>	441.1 ± 0.41 <sup>ns</sup>	89.5 ± 0.04 <sup>b</sup>	19.60 ± 0.07 <sup>ab</sup>	9.56 ± 0.12 <sup>ns</sup>
	3150 W-150 s	682.7 ± 0.47 <sup>b</sup>	441.2 ± 0.39 <sup>ns</sup>	89.8 ± 0.06 <sup>b</sup>	20.07 ± 0.12 <sup>a</sup>	9.60 ± 0.14 <sup>ns</sup>

547 Values are mean ± standard error (n=3). Different letters in the same column indicate significant differences among mean values of  
 548 different treatments (*p*<0.05). "ns" means there are no significant differences. Low MWP: Microwave pasteurization at low power  
 549 and long time. Medium MWP: Microwave pasteurization at medium power and medium time. High MWP: Microwave  
 550 pasteurization at high power and short time.

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**Table 3.** Residual activity (%RA) of peroxidase (POD), pectin methylesterase (PME), and polygalacturonase (PG) in unheated (control), conventional (CP) and microwave (MWP) pasteurized tomato puree.

	<b>Treatments</b>	<b>POD</b>	<b>PME</b>	<b>PG</b>
<b>MWP Doses</b>	Untreated	100.00 ± 0.00 <sup>a</sup>	100.00 ± 0.00 <sup>a</sup>	100.00 ± 0.00 <sup>a</sup>
	CP	15.99 ± 0.55 <sup>b</sup>	19.57 ± 0.10 <sup>b</sup>	55.77 ± 0.44 <sup>b</sup>
<b>Low</b>	390 W-848 s	15.90 ± 0.61 <sup>b</sup>	16.97 ± 0.15 <sup>c</sup>	52.05 ± 0.29 <sup>c</sup>
	510 W-805 s	15.80 ± 0.49 <sup>b</sup>	16.48 ± 0.10 <sup>c</sup>	49.43 ± 0.37 <sup>d</sup>
	770 W-460 s	15.32 ± 0.29 <sup>b</sup>	16.29 ± 0.13 <sup>c</sup>	48.33 ± 0.60 <sup>de</sup>
<b>Medium</b>	980W-340 s	14.81± 0.33 <sup>b</sup>	16.16 ± 0.05 <sup>c</sup>	47.97 ± 0.27 <sup>e</sup>
	1640 W-300 s	14.03 ± 0.78 <sup>c</sup>	16.13 ± 0.06 <sup>d</sup>	32.06 ± 0.56 <sup>f</sup>
	1700 W-230 s	13.66 ± 0.94 <sup>c</sup>	16.02 ± 0.03 <sup>de</sup>	32.84 ± 0.50 <sup>f</sup>
<b>High</b>	1900 W-180 s	12.95 ± 0.64 <sup>cd</sup>	15.02 ± 0.22 <sup>de</sup>	32.80 ± 0.52 <sup>f</sup>
	2700 W-160 s	12.26 ± 0.52 <sup>d</sup>	14.99 ± 0.07 <sup>de</sup>	30.51 ± 0.56 <sup>g</sup>
	3150 W-150 s	11.72 ± 0.82 <sup>e</sup>	14.65 ± 0.10 <sup>e</sup>	29.22 ± 0.52 <sup>g</sup>

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Values are mean ± standard error (n=3). Different letters in the same column indicate significant differences among mean values of different treatments ( $p < 0.05$ ). Low MWP: Microwave pasteurization at low power and long time. Medium MWP: Microwave pasteurization at medium power and medium time. High MWP: Microwave pasteurization at high power and short time.